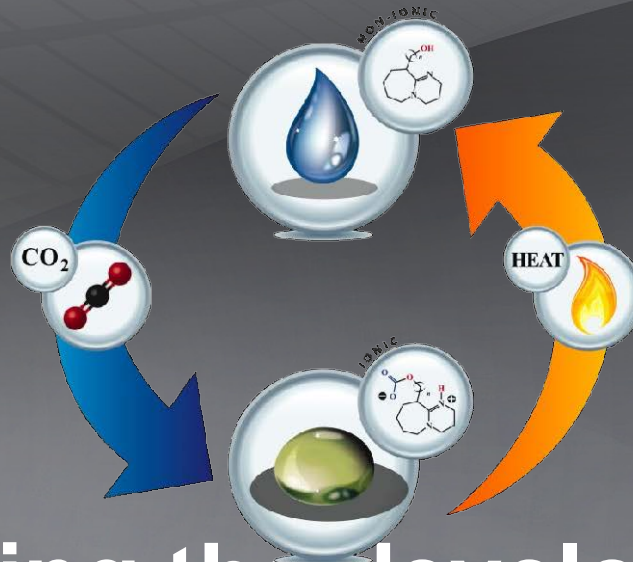




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Accelerating the development of transformational solvent systems for CO₂ separations

FWP 65872

DAVID J. HELDEBRANT
NETL CO₂ CAPTURE TECHNOLOGY MEETING
PITTSBURGH, PA
AUGUST 11, 2016

PNNL at a Glance



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FY15:
\$955 MILLION
in R&D expenditures

FY15:
4,400 STAFF

98
R&D 100 AWARDS

81
Tech transfer AWARDS

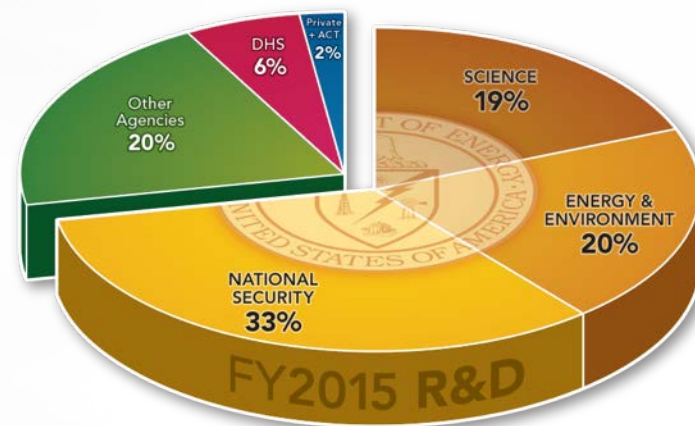
Intellectual property and startups

Average
ONE
INVENTION
per day

Average
ONE
PATENT
per week

822
LICENSES
since 1970s

170+
BUSINESSES
started with
PNNL IP
or executives



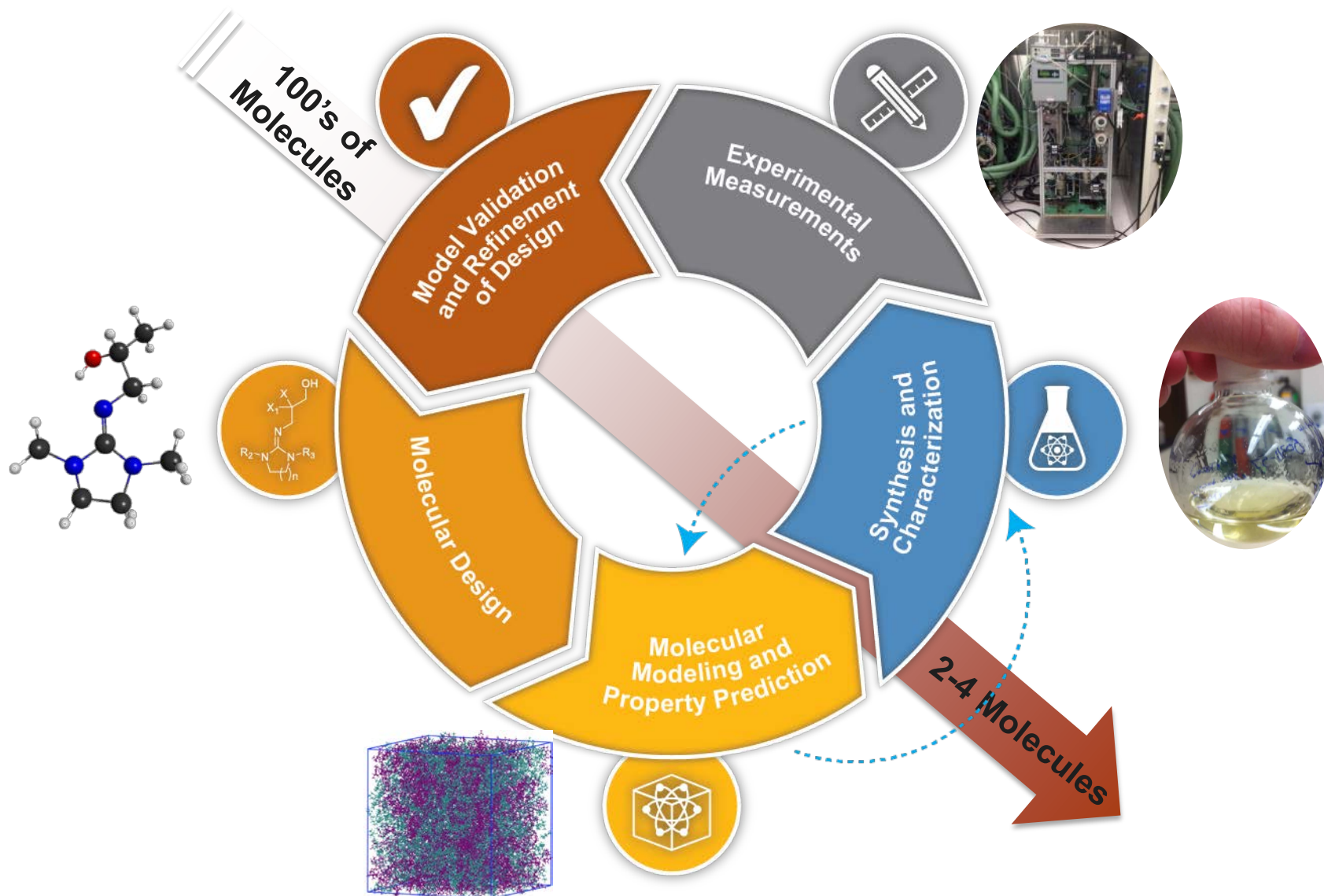
Overview: Integrating Molecular Design, Synthesis & Testing For Multiple Platforms



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**Aiding DOE's transformational solvent portfolio address the grand challenge of viscosity*



Project Goals and Objectives

Objective

- ▶ Enable advanced solvent designs for all water-lean solvents up DOE's TRL readiness scale to enable large scale testing and deployment by year 2030.

Goals

- ▶ Develop a reduced order viscosity model that can predict key solvent physical and thermodynamic properties
- ▶ Down-select hundreds of candidate molecules to 2-4 viable derivatives
- ▶ Design testing devices for expedited testing of candidate solvents
- ▶ Collect necessary additional thermodynamic and kinetic data to validate models
- ▶ Partner with technology owners to advance the field of water-lean solvents

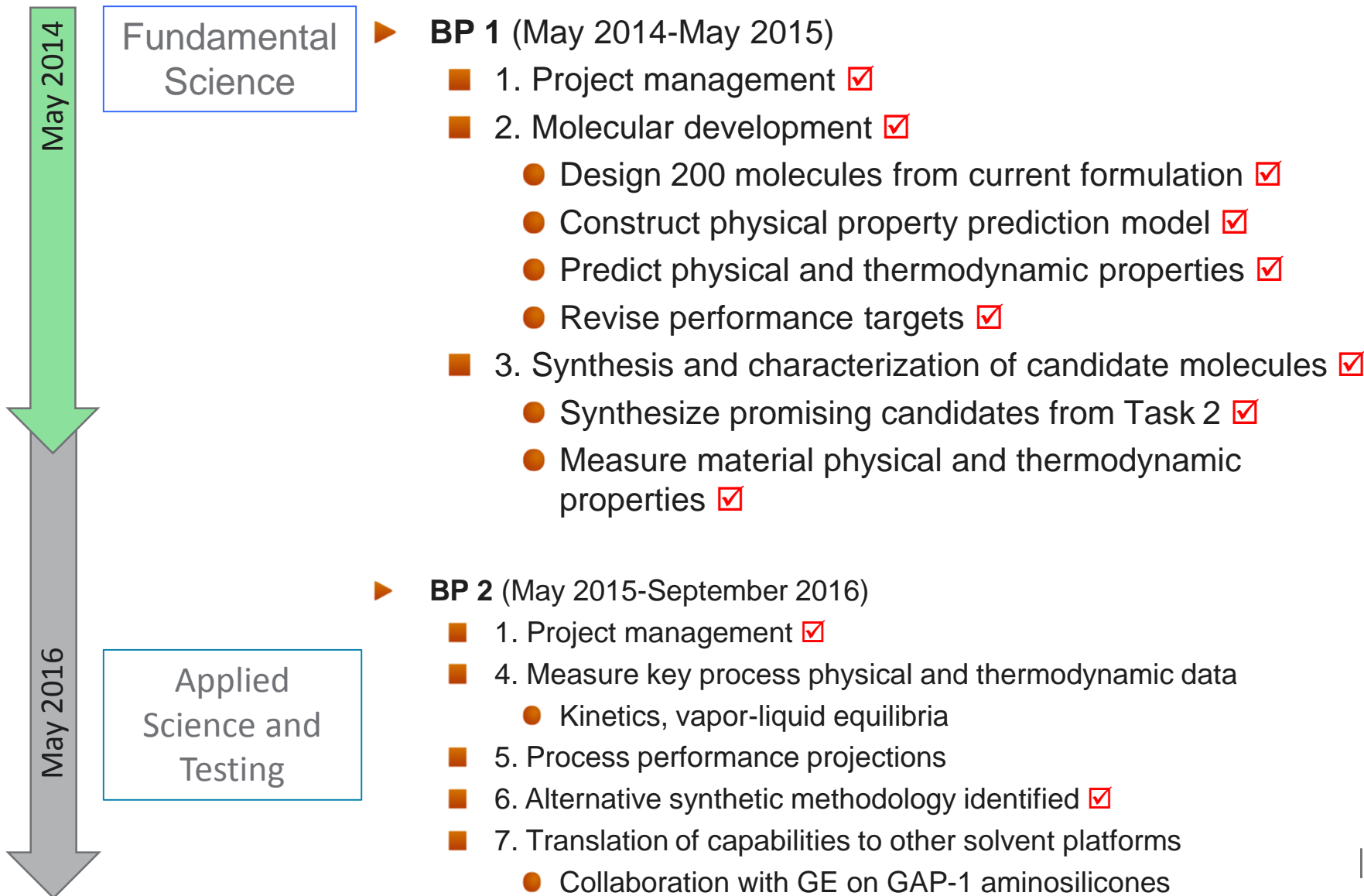
Project Schedule and Major Tasks



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Funding: \$2,561,000 / 24 months

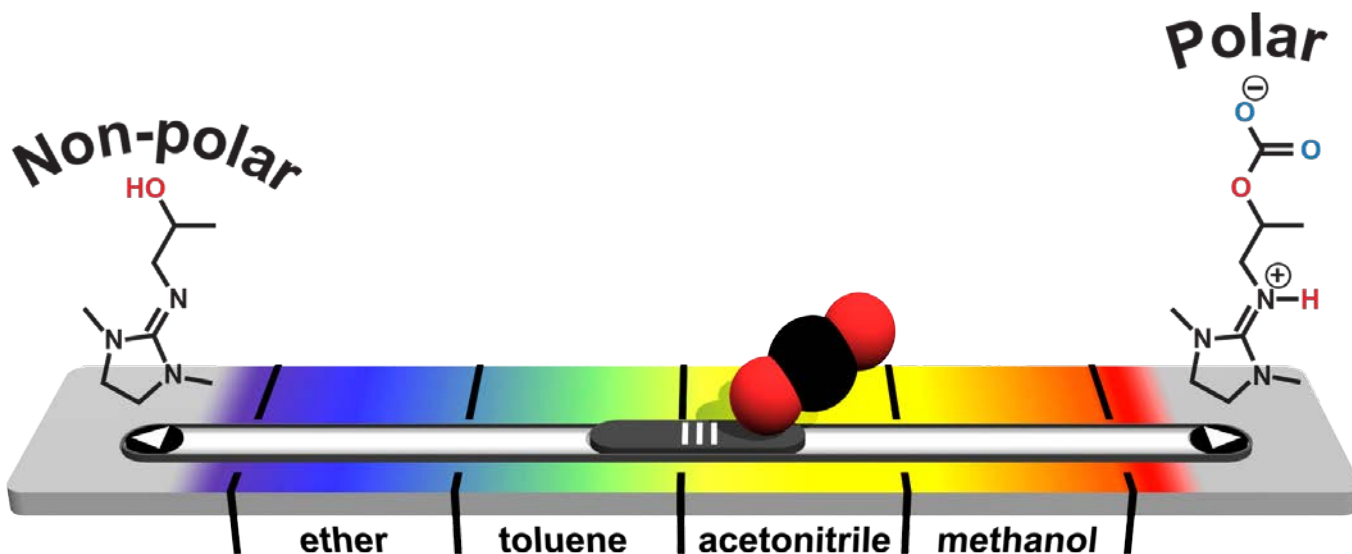


Case Study: CO₂-Binding Organic Liquids (CO₂BOLs)



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*Nile Red Solvatochromatic Polarity Scale

- “Water-lean” organic switchable ionic liquid solvent system
 - Optimal water level in circulating solvent estimated
 - (~5 wt. % water confirmed by simulation)
 - Heat of solution -80 kJ/mol (similar to amines @ -85 kJ/mol)
 - CO₂BOL material projected at (\$35-70/kg)

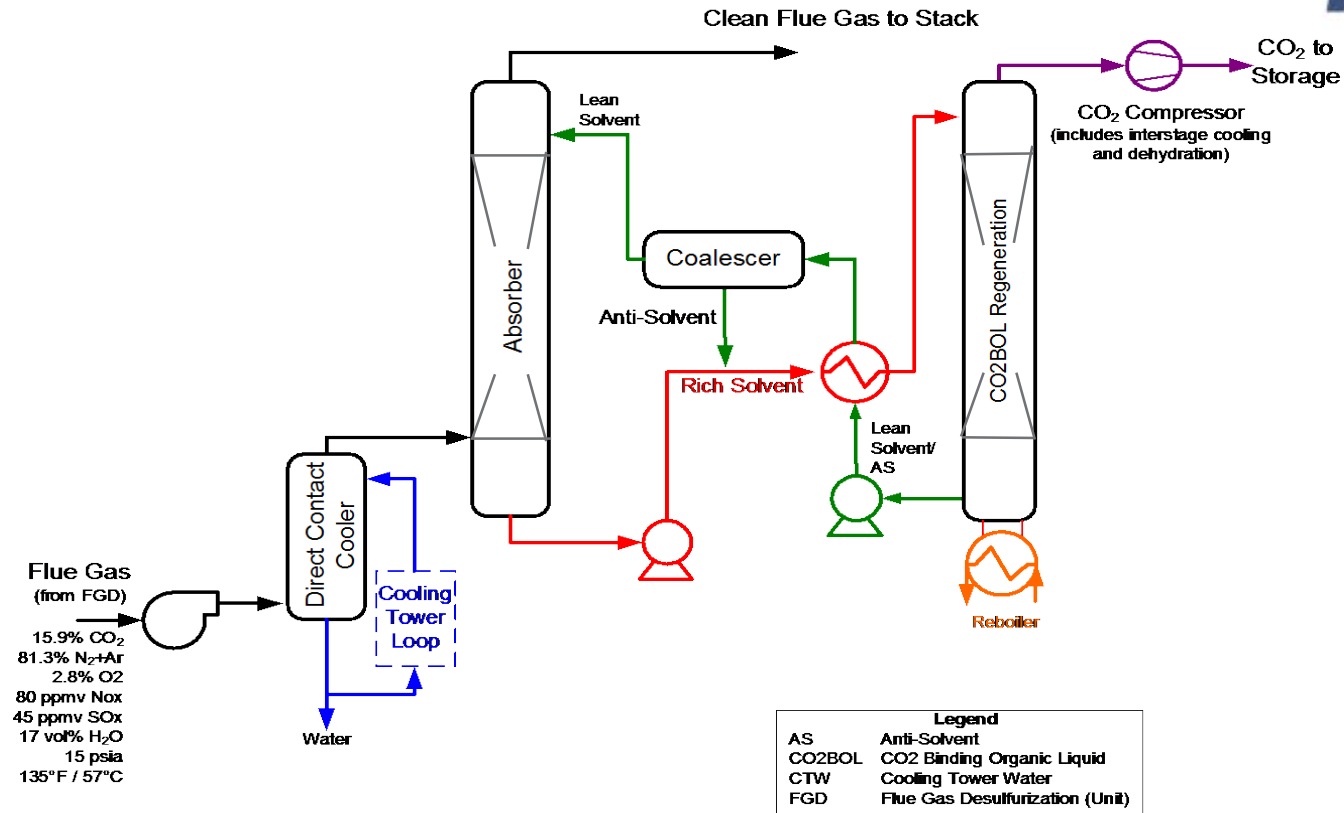
CO₂BOL/PSAR Conceptual Configuration



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FLUOR[®]



- Similar to aqueous amine systems except:
 - Coalescing tank
 - Antisolvent loop
 - Water management equipment
- Commercially available equipment and infrastructure

CO₂BOLs/PSAR Could be Energetically Viable With Lower Solvent Viscosities

	MEA (Recreated NETL Case 10)	CO ₂ BOL/PSAR (356 cP)	CO ₂ BOL/PSAR (578 cP)	CO ₂ BOL/PSAR (20 cP Target)
Rich solvent loading (mol CO₂/mol solvent)	0.49	0.28	0.34	0.50
Temperature Required for Regeneration (°C)	120	104	104	85
Estimated Reboiler Duty (BTU/lb CO₂)	1,520	1,107	965	870
Increase in Net Electric Power over Case 10 (%)	0	7	9	16

- Viscosity limits the possible *rich* solvent CO₂ loadings and reboiler duty
- If a 20 cP target were achieved:
 - Reboiler duties as low as 870 btu/lb CO₂, (57% of Case 10)
 - 16% increase in net power at an equivalent coal feed rate

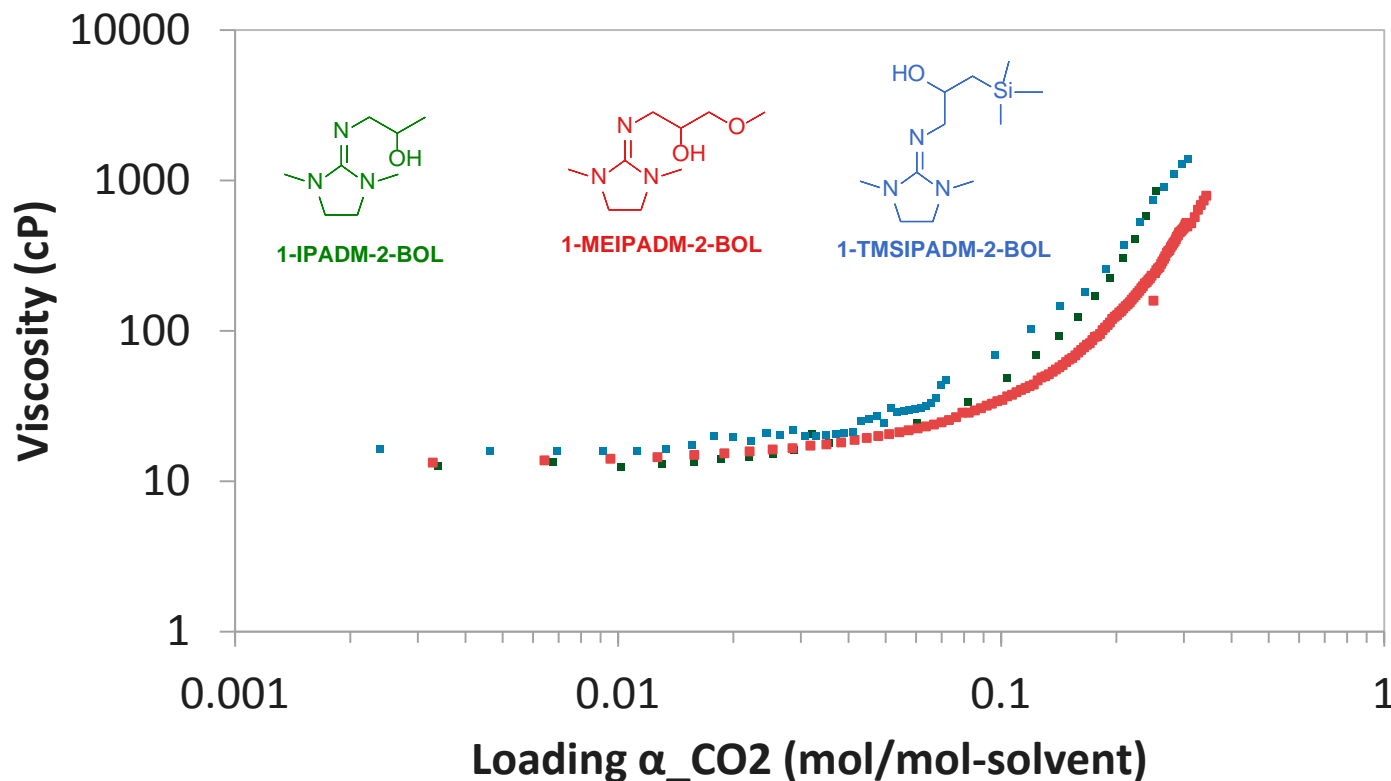
Cycle-1 Showed Significant Reductions in Viscosity



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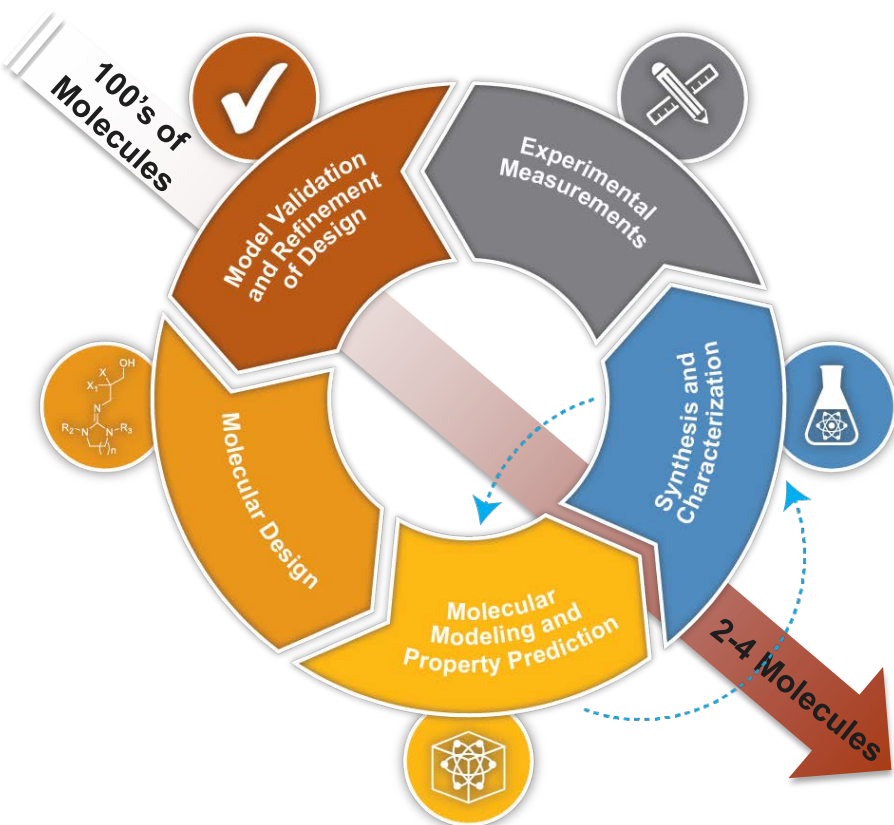
- ▶ Down-selected from >350 molecules to 13 variants for each viscosity reducing factor
 - Internal H-bond and cation charge solvation (ether) show most promise
- ▶ 60% reduction in viscosity for MEIPADM-2-BOL
- ▶ Experimental data used to validate molecular models



3,000 cP for IPADM-2-BOL @ 50 mol% CO₂ loading
1,100 cP for MEIPADM-2-BOL @ 50 mol% CO₂ loading

Technical Approach: CO₂BOL Solvent Class Cycle-2

Using PNNL's infrastructure for 2nd level refinement of CO₂BOLs



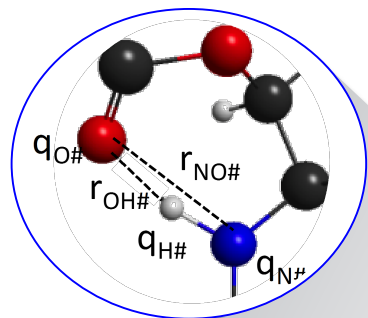
- Down-select variants from Cycle-1 derivative
- Use reduced viscosity model that enables viscosity prediction off an optimized structure
- Perform comprehensive solvent property testing using Δ PVT cell

Reduced Model Is Qualitatively Predicting Viscosity From Optimized Structures



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$$X = \frac{q_N q_O}{r_{NO}} - \frac{q_O q_H}{r_{OH}} \quad (1)$$

$$P_{int} = c_1 X + c_2 \quad (2)$$

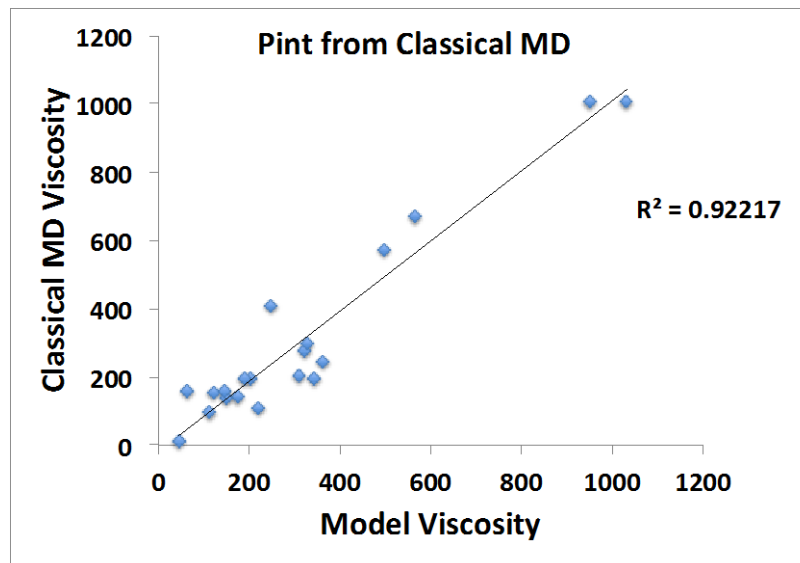
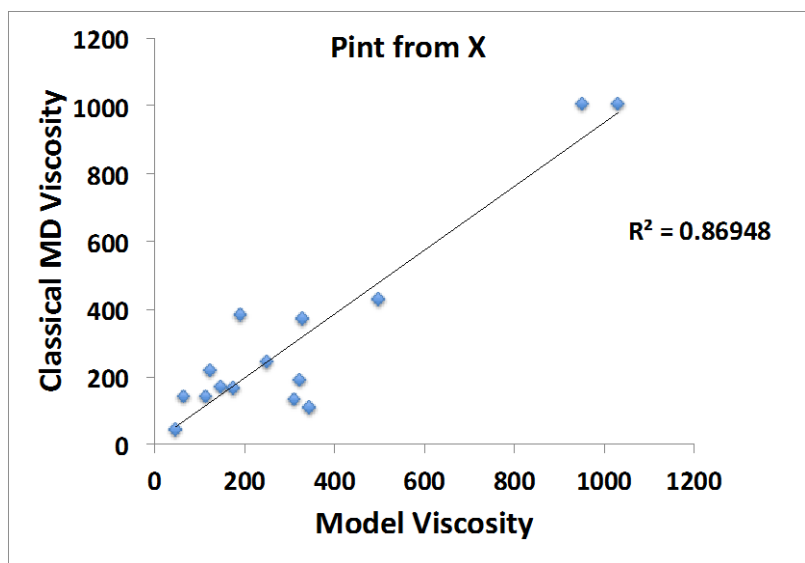
$$\eta = c_1 \ln \left(\frac{P_{int}}{1 - P_{int}} \right) \exp(c_2 L) \quad (3)$$

η : viscosity

P_{int} : percent internal hydrogen bond, calculated as a function of X

L: mol percent CO₂ loading

c_1 & c_2 : constants to obtain the viscosity magnitude in cP, varied to fit the *experimental* data for at 0 and 25 mol% CO₂



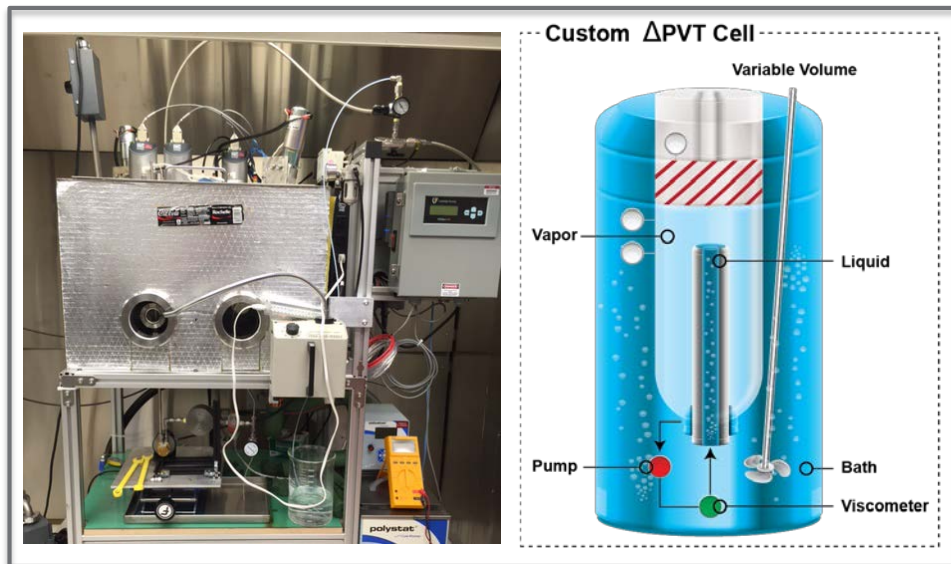
PNNL's Custom Δ PVT Cell Enables Rapid Screening

**Standardized Measurements on ~40 mL scale*

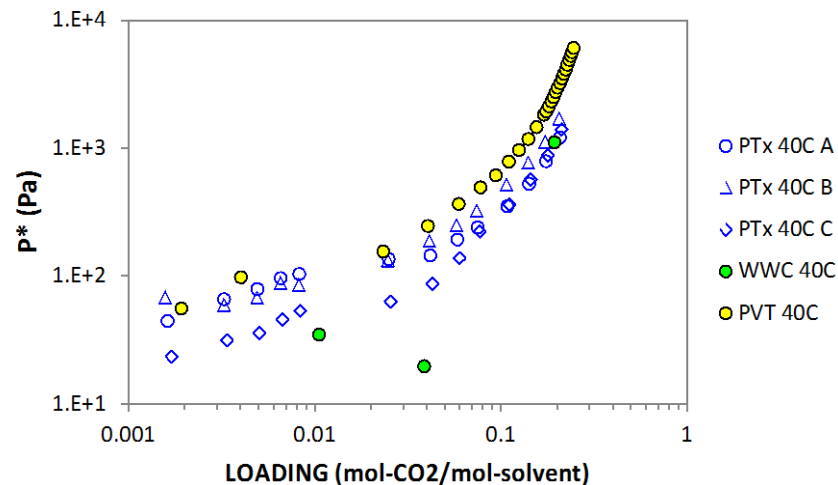


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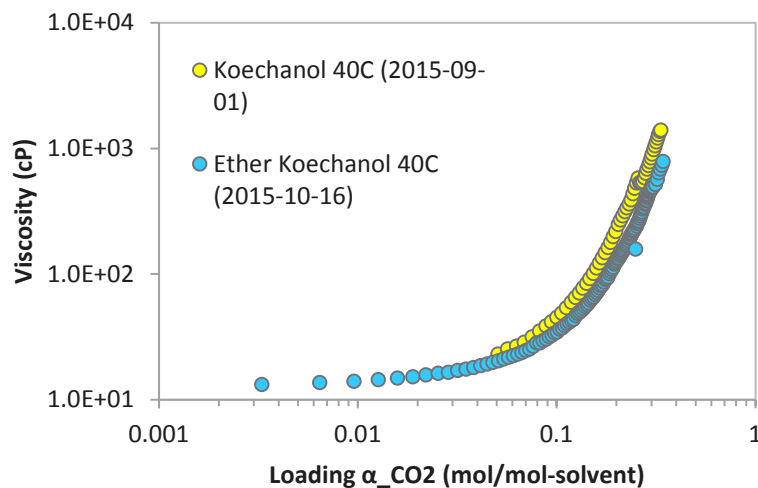
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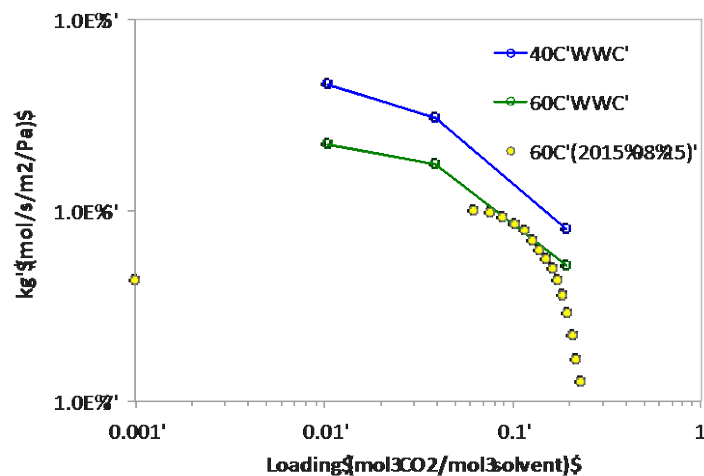
▶ PT_x Capability Matches VLE



▶ Flow-through viscometer measures cP as a function of CO₂ loading



▶ Miniaturized wetted wall contactor can extract qualitative kg' data



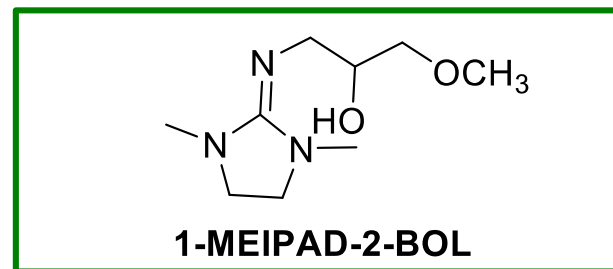
Applying Molecular Design Towards CO₂BOL Cycle-2

What we learned from Cycle-1:

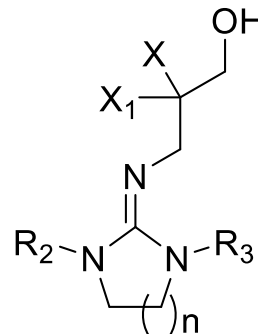
- ▶ High degree of internal hydrogen bonding
- ▶ Ether groups for cation charge solvation
- ▶ Potential for neutral capture

Viscosity Modifying Factors:

- ▶ Fine tuned electronics for acid/base equilibria
- ▶ Steric crowding to reduce stacking

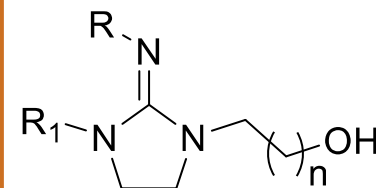


Electronic Effects



X and X₁ = F, Cl, CF₃,
(EWG) or OMe, CH₂NMe₂,
(EDG) and R₂=R₃=Me,
CF₃, CF₃CF₂, OMe with
n=1, 2, 3

Steric Effects



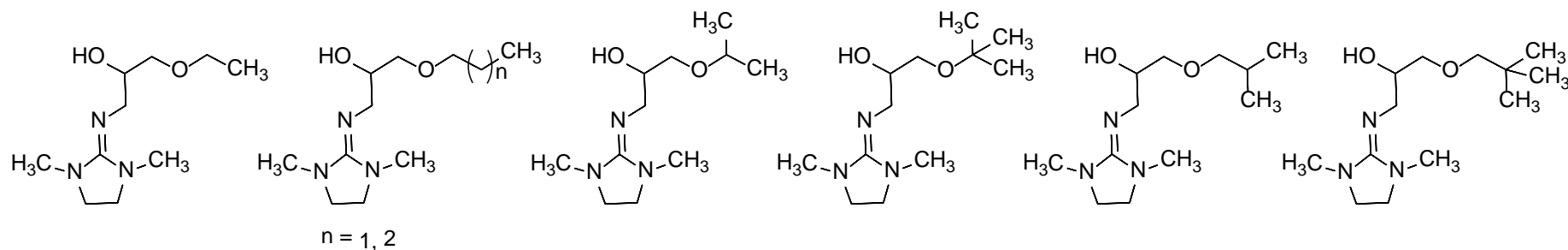
R=Pr, *i*-Pr, Bu, *t*-Bu
R₁=Me, Et, *i*-Pr
with n=1, 2, 3

Reduced Model Predicts ~90% Reduction for Multiple Derivatives (@ 25 mol% CO₂)



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275

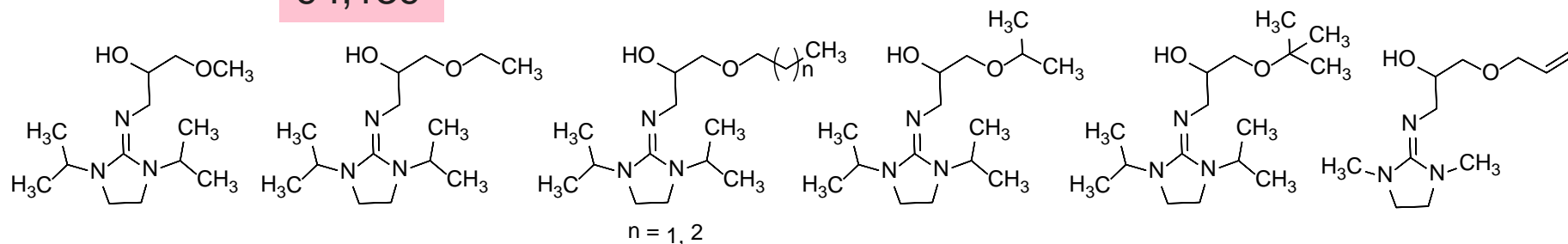
94,139

228

170

111

146



36

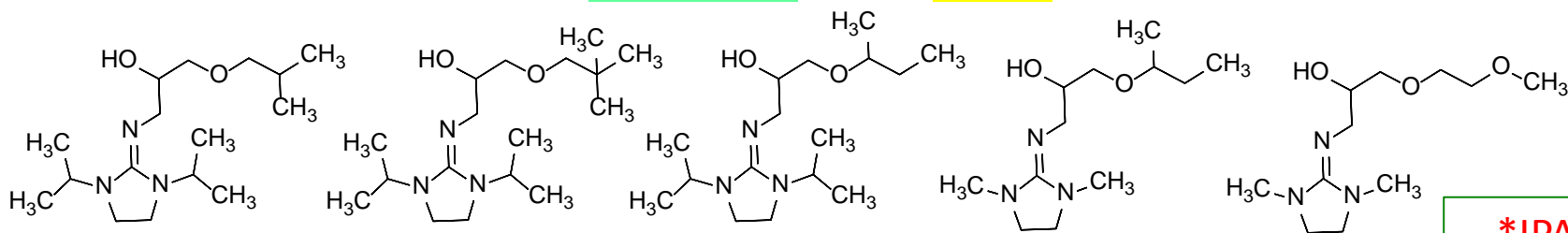
13

n/a, 14

33

29

n/a



14

n/a

14

145

198

***IPADM-2-
BOL = 150 cP**

Synthesis & Testing of Cycle-2 Derivatives Confirms Significant Viscosity Reduction

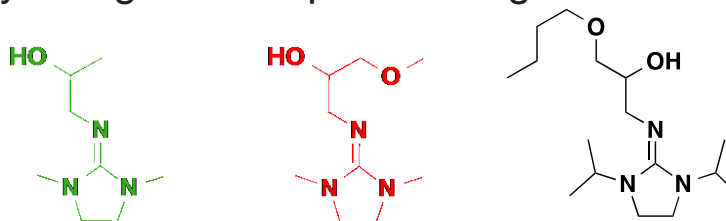


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- ▶ Synthesizing 4 variants of MEIPADM-2-BOL with ether and isopropyl moieties
 - 90% reduction predicted @ 25 mol% CO₂, 40 °C
- ▶ BEIPADIPA-2BOL currently being scaled up for testing

IPADM-2-BOL @ 40 mol% CO₂
MEIPADM-2-BOL @ 35 mol% CO₂
BEIPADIPA-2-BOL @ 42 mol% CO₂



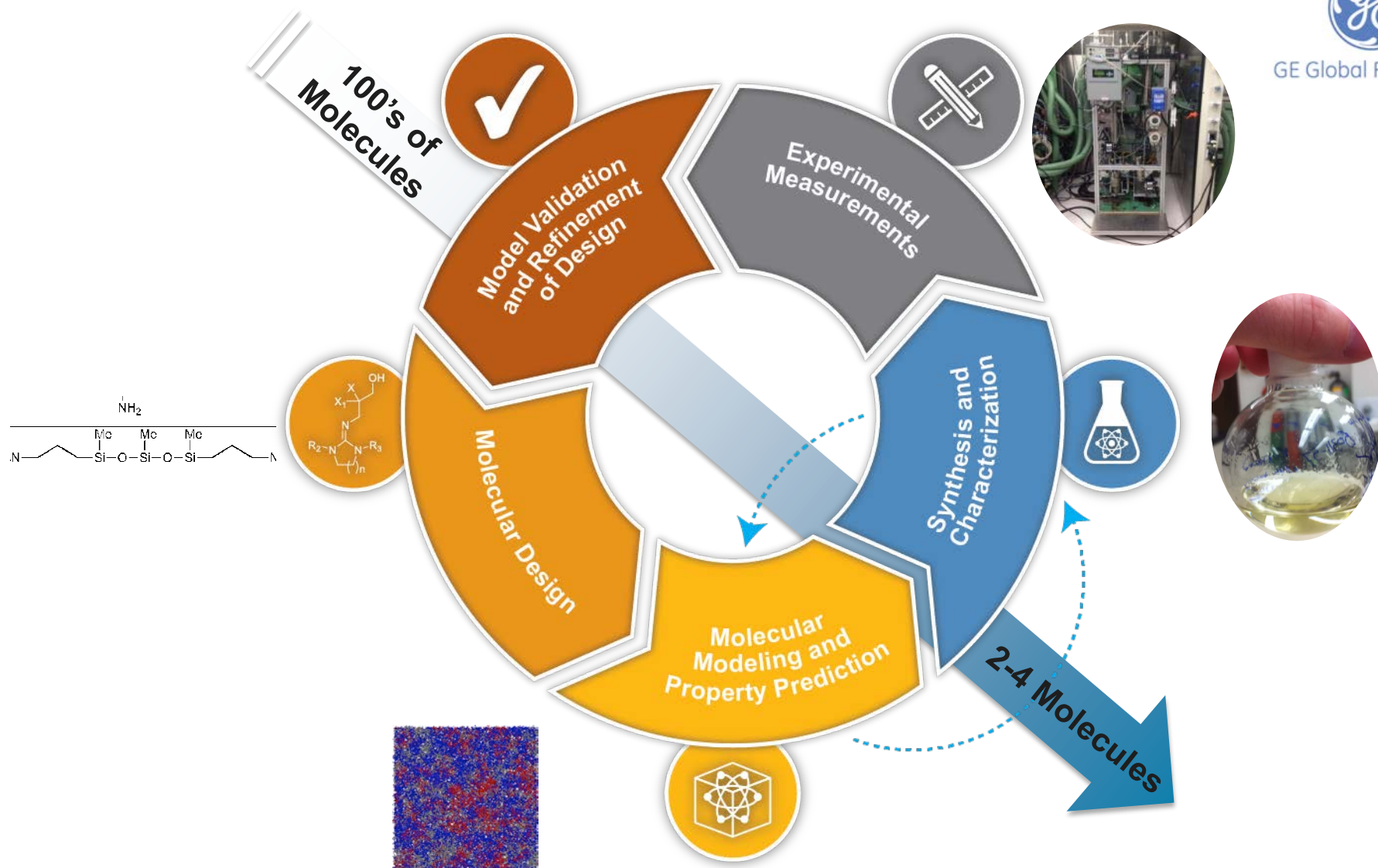
100
Molecules

2-4 Molecules

Integrating Molecular Design, Synthesis & Testing For Aminosilicone Solvents



**Collaboration with GE Global Research*



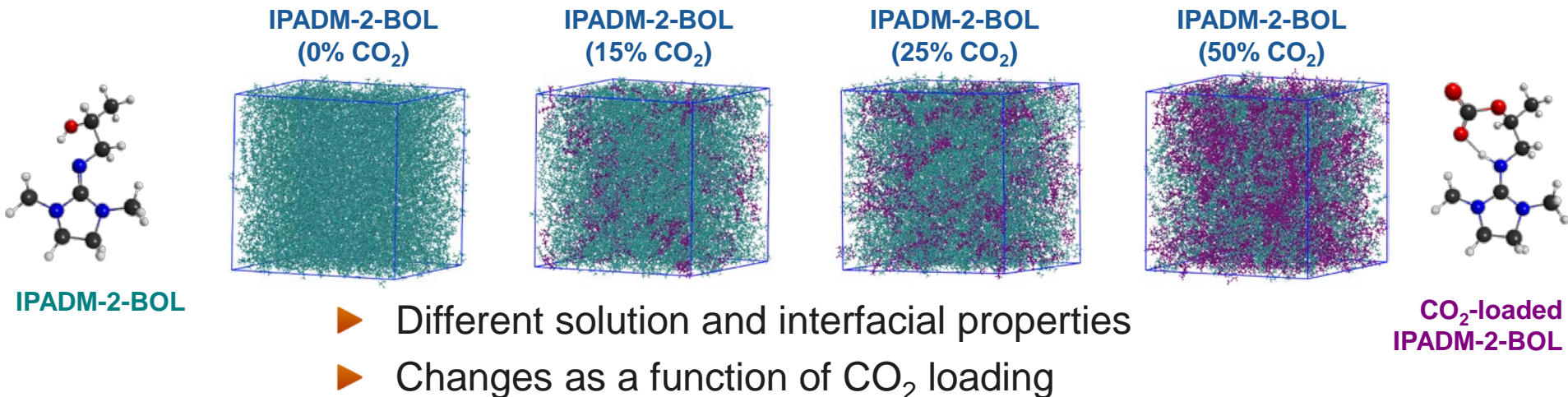
All Non-Aqueous Solvents May Have “Heterogeneous” Molecular Structure



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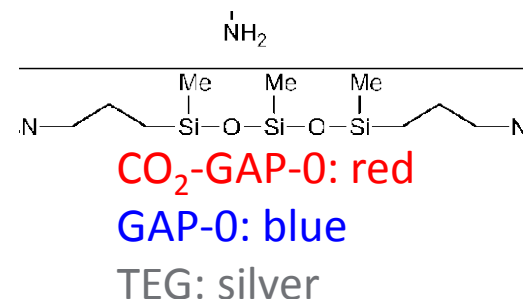
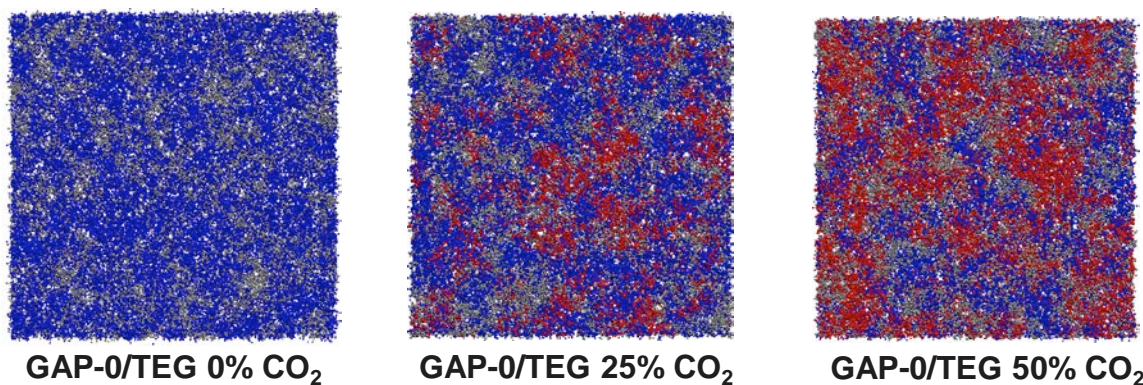
CO₂BOL Solvent Class: (100% Concentrated)



Aminosilicone Solvent Class: (Triethylene Glycol co-Solvent)²



GE Global Research

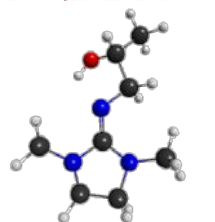
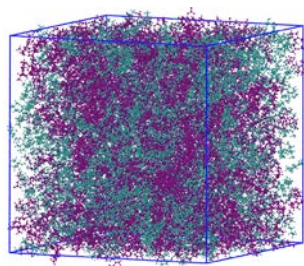


- ▶ TEG may not be dissolving GAP carbamates
- ▶ Potential for different co-solvent

Heterogeneous Molecular Structure May Account for Similar Materials Performance

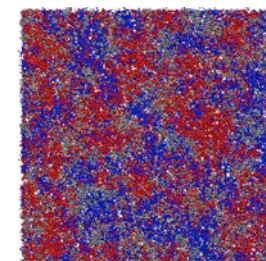
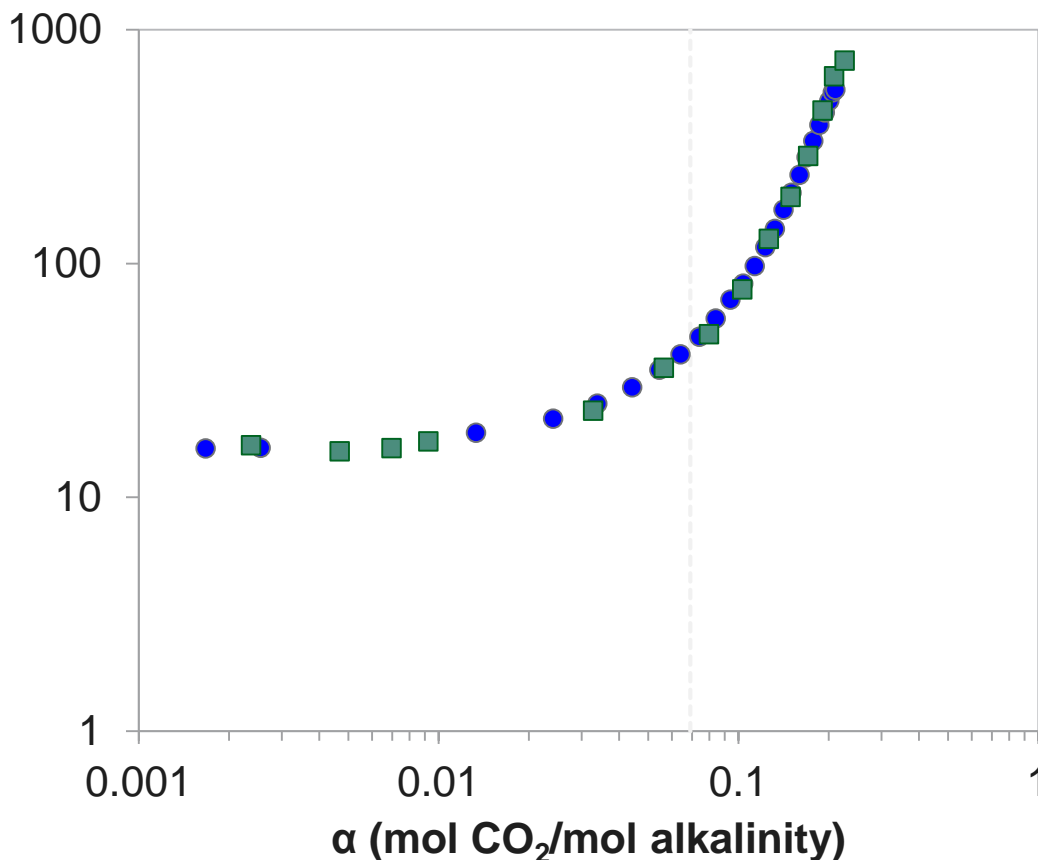


- ▶ CO₂BOLs and aminosilicones show similar predicted solvent structure and viscosity profiles as a function of CO₂ loading



IPADM-2-BOL

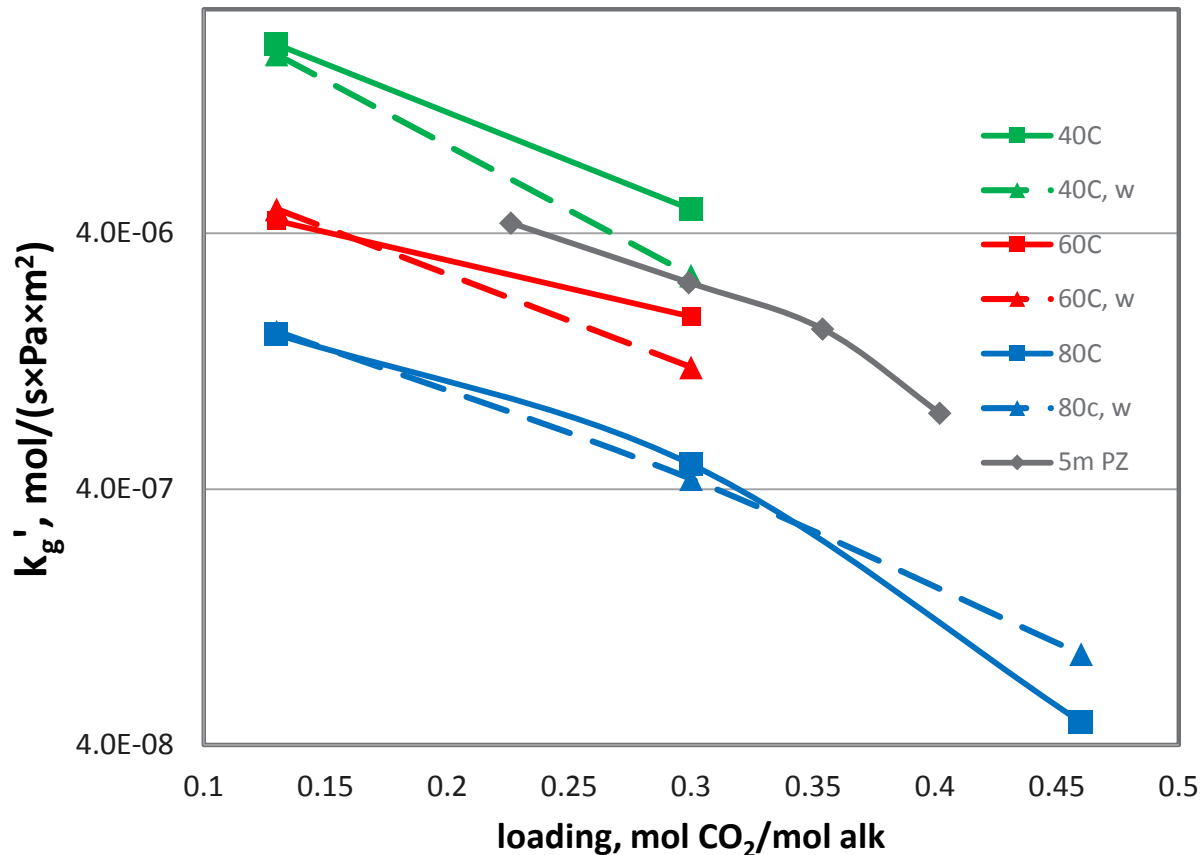
□ (cP)



GAP-1/TEG

Mass Transfer of GAP-1/TEG is Inverse With Temperature

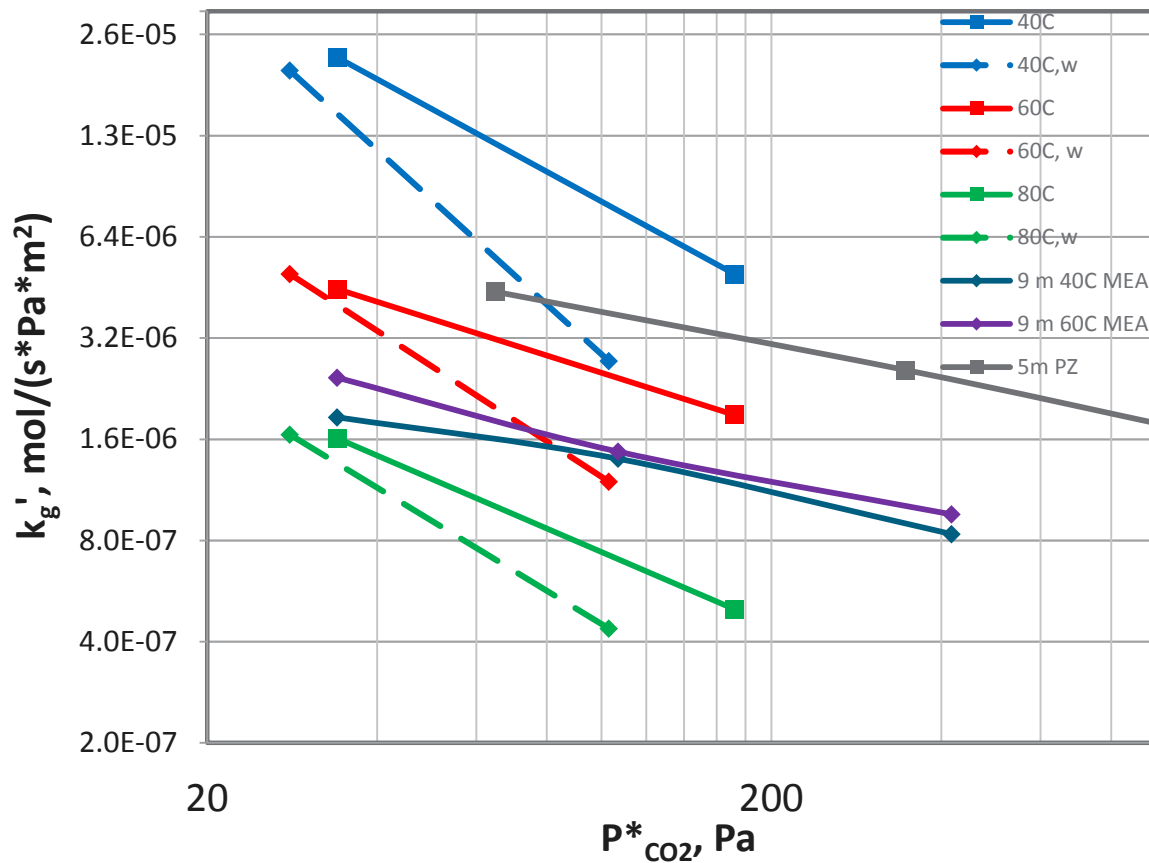
- ▶ Inverse k_g' with temperature observed
 - Similar to IPADM-2-BOL¹
- ▶ Follows trend of physical solubility of CO₂ driving liquid-stage kinetics



1) Whyatt et al. ChemSusChem, 2015, 8, (21), 3617, 2) Whyatt et al., Manuscript in preparation

Mass Transfer of GAP-1/TEG is Greater Than MEA & Piperazine

- ▶ k_g' of GAP-1 is twice that of 8 m PZ and 6 times that of 9 m MEA
 - 100 Pa of $P^*_{CO_2}$ at 40 °C
- ▶ Non-aqueous k_g' values larger at higher solution viscosities¹



Strategies of Refinement of GAP-1 Derivatives



****GAP-1/TEG shows enhanced kinetics compared to aqueous solvents though viscosity can still be lowered***



Near Term

- ▶ Identify co-solvents that dissolve ionic clusters
- ▶ Identify potential diluents to breakup ionic clustering

Long Term

- ▶ Apply findings from CO₂BOL solvent class to refine GAP derivatives
 - Promote internal H-bonding
 - Add ether groups for charge solvation
 - Increase steric bulk
 - Optimize acid/base equilibria

Benefits of Technology to the Program



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- An approach that can benefit all solvent classes
- Rapid modeling and testing of all CO₂ binding mechanisms
- Detailed understanding of molecular level interactions and how they impact performance

	Alkylcarbonate-Derived	Carbamate-Derived	Imidazole-Derived
	$R-O-CO_2^{\ominus}$	$R-NHCO_2^{\ominus}$	$R-N \begin{array}{c} \diagup \\ \diagdown \end{array} N^{\oplus}-CO_2^{\ominus}$
Property	(CO ₂ BOLs)	(RILs, Aminosilicones, TSILs, Phase-Change)	(imidazole, carbene, AHA ILs)
Internal H-Bonding	[Green arrow from Alkylcarbonate to Imidazole-Derived]		
Molecular Stacking	[Green arrow from Alkylcarbonate to Imidazole-Derived]		
Steric Crowding	[Green arrow from Alkylcarbonate to Imidazole-Derived]		
Optimized Thermo-chemistry	[Green arrow from Alkylcarbonate to Imidazole-Derived]		
Quantify k_g'	[Green arrow from Alkylcarbonate to Imidazole-Derived]		

KEY

Current Work

Projected Translation

Next Steps: FY17 Work Scope



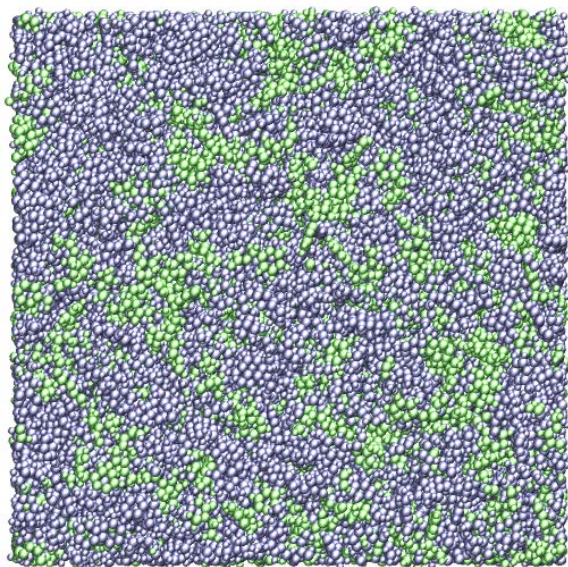
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Three parallel efforts at each level of testing and development

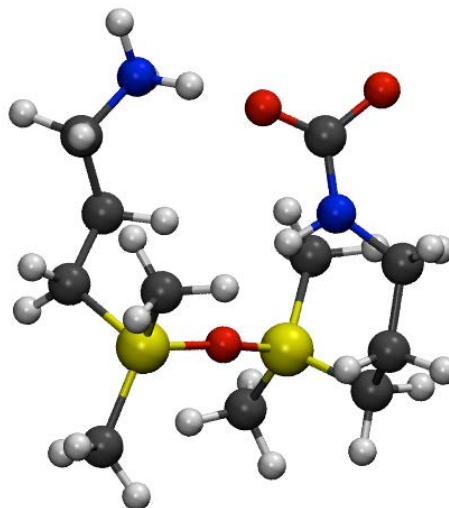


**Solvent Class #3
Molecular Development
Cycle 1**



Development of model
Initial solvent screen

**Aminosilicone
Molecular Development
Cycle 2**



Molecular-level refinement
Reduce viscosity by up to 90%

**CO₂BOL/PSAR
Continuous Flow
Testing for TEA**



Validate performance
\$40/ton CO₂ target

Acknowledgements

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Andy Aurelio, Lynn Brickett, John Litynski



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Dr. Phillip Koech



Dr. Vanda Glezakou
Dr. Roger Rousseau



Dr. Feng Zheng



Solvent Design
Retrosynthetic-
analysis
Synthesis & Scaleup



Dr. Deepika Malhotra

Computational
Modeling
Physical property
projections



Dr. David Cantu

Materials
Testing
& Analysis



Greg Whyatt
Charles Freeman



Andy Zwoster

Process
Modeling
Performance
Projections



Mark Bearden

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GE Global Research

Dr. Robert Perry
Tiffany Westendorf
Benjamin Wood

Lawrence Livermore
National Laboratory

Dr. Josh Stohlaroff,
Dr. John Vericella

EPRI | ELECTRIC POWER
RESEARCH INSTITUTE

Abhoyjit Bhowan |

*Advisory process engineering,
thermodynamics:
Dr. Paul M. Mathias

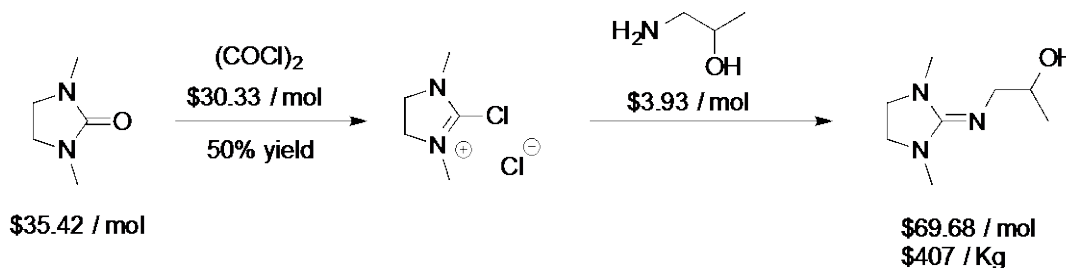
Revised Synthetic Pathway and Cost for Optimal Derivative May Achieve Cost Targets



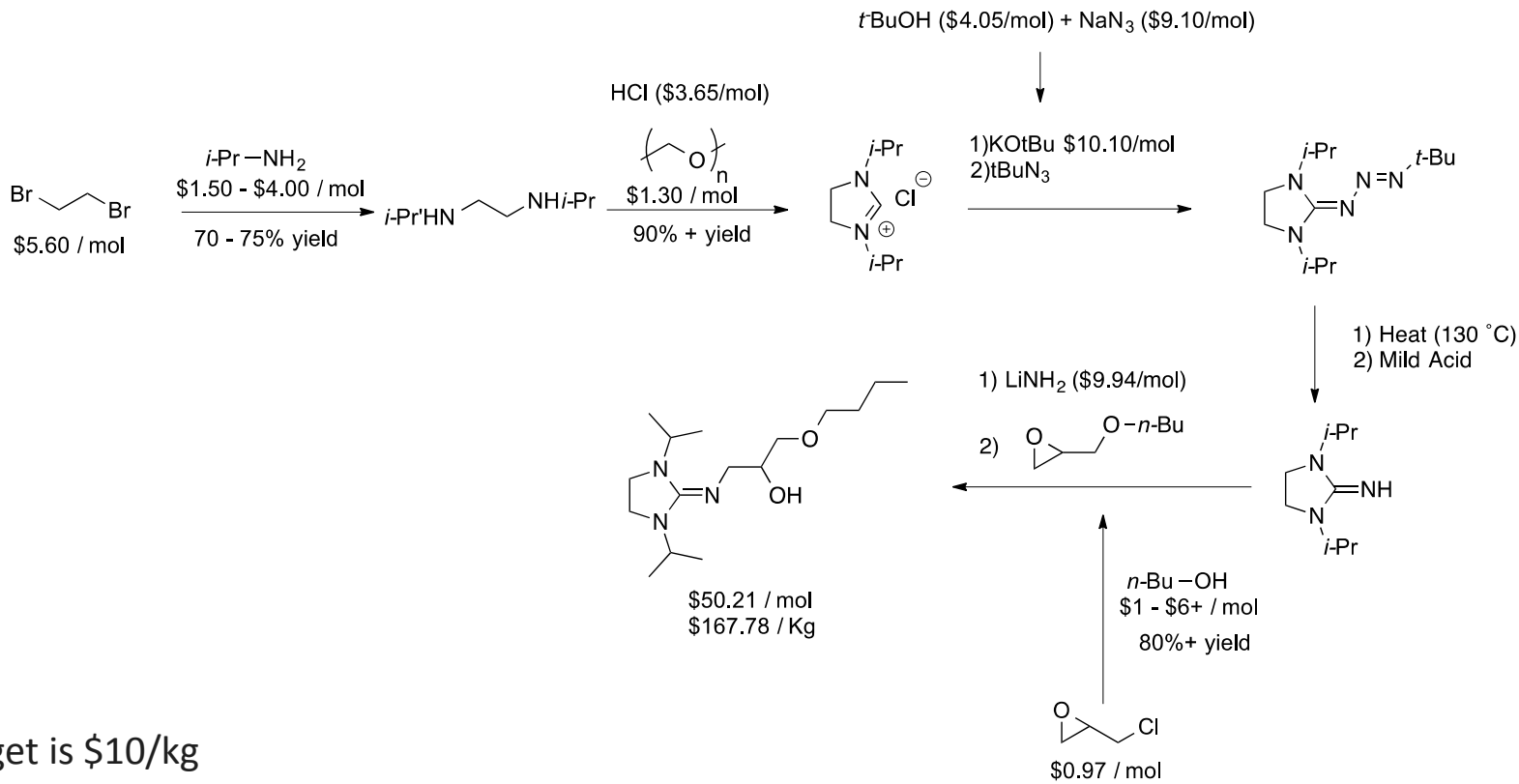
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- ▶ IPADM-2-BOL costs \$407/kg, but projected \$35/kg at tonnage scale

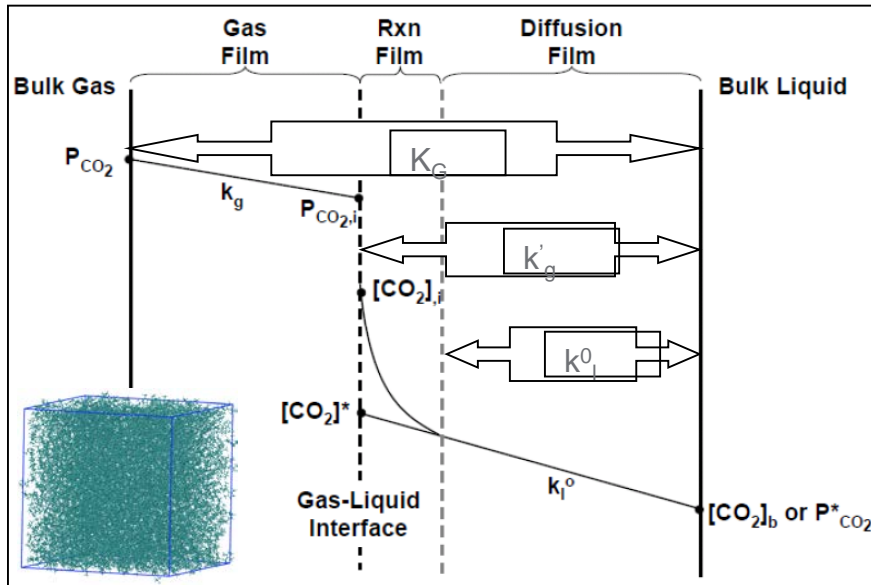


- ▶ BEIPADIPA-2-BOL costs \$168/kg, but projected at \$12/kg at tonnage scale

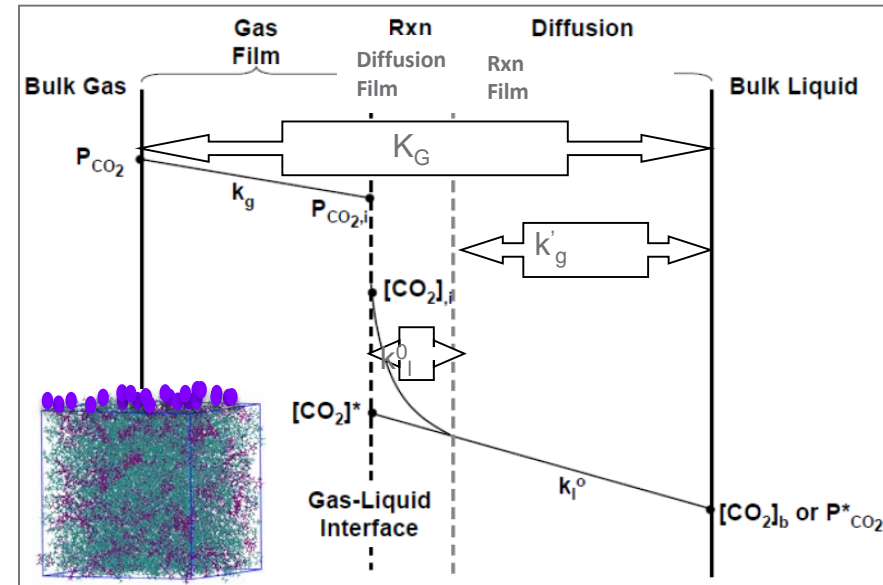


*Cost target is \$10/kg

Impacts of a Heterogeneous Solvent Structure - Collaboration With CCSI



Aqueous Profile



CO₂BOL Profile

- ▶ Aqueous solvents have a reactive interface, a diffusion film, then bulk liquid.¹
- ▶ CO₂BOLs have a diffusion film (passivated interface) followed by a reaction film, then bulk liquid.²
- ▶ Potential new diffusion routes and mechanisms of CO₂ and CO₂-containing ions
- ▶ Different contactor or packing may be needed New film theories needed to quantify this behavior

Utilizing A Heterogeneous Solvent -Collaboration With CCSI



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- ▶ Gradient packing to adjust to changing fluid
 - Changes in fluid properties: contact angle, surface tension and viscosity
 - Changes in packing: Structured to random, packing material

